

Aerodynamics

Turbulent Flow Mean velocity profile, U

1. Linear profile in the linear (laminar) sub-layer, $y^+ < 5$

$$U^+ = y^+$$

2. Semi-logarithmic profile in wall (log) law,
 $y^+ > 30 - 50, \quad y < 0,1 - 0,2\delta$

$$U^+ = \frac{1}{\kappa} \ln(y^+) + C \quad k = 0,41 \quad C \cong 5,2$$

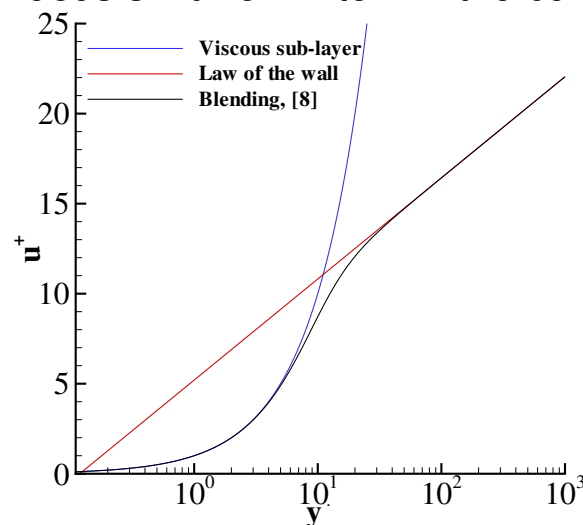
3. Continuous shift from 1 to 2 in the buffer-layer

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Turbulent Flow Mean velocity profile, U

3. Continuous shift from 1 to 2 in the buffer-layer

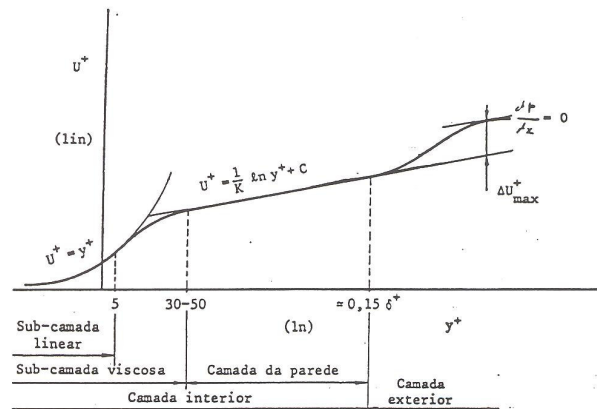


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 Turbulent Flow
 Mean velocity profile, U

4. Outer part of the profile where the velocity tends to U_e^+ defined from the difference to the log-law



$$U_e^+ = \frac{U_e}{u_\tau} = \sqrt{\frac{2}{C_f}}$$

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 Turbulent Flow
 Mean velocity profile, U

- Wake component

$$\Delta U^+ = U^+ - \left(\frac{1}{\kappa} \ln(y^+) + C \right) = \frac{\Pi}{\kappa} w \left(\frac{y}{\delta'} \right)$$

- Coles (empirical) wake profile

$$w \left(\frac{y}{\delta'} \right) = 1 - \cos \left(\pi \frac{y}{\delta'} \right)$$

- $y = \delta'$ is the location where the maximum difference to the log law occurs

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Mean velocity profile, U

- Wake component magnitude/intensity

$$\Delta U_{\max}^+ = 2 \frac{\Pi}{\kappa}$$

- Mean velocity profile outside the viscous sub-layer

$$U^+ = \frac{1}{\kappa} \ln(y^+) + C + \frac{\Pi}{\kappa} \left(1 - \cos\left(\pi \frac{y}{\delta'}\right) \right)$$

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Self-preserved flows

- von Kármán's integral equation

$$\frac{d}{dx} (\rho U_e^2 \theta) = \tau_w + \delta^* \frac{dP}{dx}$$

- History/memory parameter

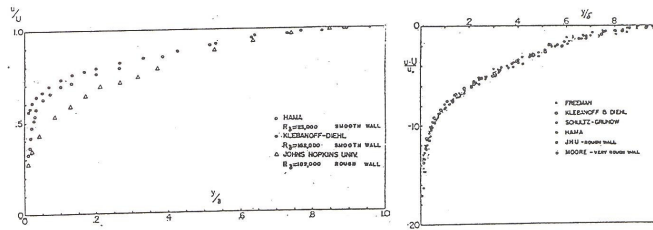
$$\beta = \frac{\delta^*}{\tau_w} \frac{dP}{dx}$$

- Self-preserved flow, $\beta = \text{constante}$

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Turbulent Flow

Self-preserved flows



- Clauser's equilibrium parameter

$$G = \sqrt{\frac{2}{C_f} \frac{H-1}{H}} = \frac{\int_0^h \left[\frac{U_e - U}{u_\tau} \right]^2 dy}{\int_0^h \left[\frac{U_e - U}{u_\tau} \right] dy}$$

- G is constant for zero pressure gradient and sufficiently large Reynolds number

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Turbulent Flow

Simplified forms of the mean velocity profile

- Power-law profile

$$\frac{U}{U_e} = \left(\frac{y}{\delta} \right)^{\frac{1}{n}}$$

- Integral parameters

$$\frac{\delta^*}{\delta} = \frac{1}{n+1} \quad \frac{\theta}{\delta} = \frac{n}{(n+1)(n+2)} \quad H = 1 + \frac{2}{n}$$

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Simplified forms of the mean velocity profile

- Power-law profile $\frac{U}{U_e} = \left(\frac{y}{\delta}\right)^{\frac{1}{n}}$
 1. It does not satisfy the linear sub-layer
 2. It does not satisfy the wall (log) law
 3. $\frac{\partial U}{\partial y} \neq 0$ at $y = \delta$
 4. $\frac{\partial U}{\partial y} = \infty$ at $y = 0$

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Simplified forms of the mean velocity profile

- Power-law profile $\frac{U}{U_e} = \left(\frac{y}{\delta}\right)^{\frac{1}{n}}$
 - From experimental data:

$$\frac{dP}{dx} = 0 \rightarrow n \approx 7$$

$$\frac{dP}{dx} < 0 \rightarrow n \approx 7-10$$

$$\frac{dP}{dx} > 0 \rightarrow n \approx 3-7$$

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Zero pressure gradient (flat plate) boundary-layer

- Integration of von Kármán's integral equation

$$\frac{d\theta}{dx} = \frac{\tau_w}{\rho U_e^2}$$

- Power-law profile

$$\frac{U}{U_e} = \left(\frac{y}{\delta}\right)^{\frac{1}{7}}$$

- τ_w from a friction law for fully-developed flow in pipes

$$\lambda = \frac{4\tau_w}{1/2\rho U_{med}^2} = 0,3164 R_e^{-1/4} \quad R_e = \frac{U_{med} D}{\nu}$$

$$U_{med} = 0,8U_{max} \quad \delta \approx R \quad U_e \approx U_{max}$$

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Zero pressure gradient (flat plate) boundary-layer

- Shear-stress at the wall

$$\frac{\tau_w}{\rho U_e^2} = 0,0225 \left(\frac{\nu}{U_e \delta}\right)^{\frac{1}{4}}$$

- von Kármán's integral equation with δ as the dependent variable

$$\frac{7}{72} \frac{d\delta}{dx} = 0,0225 \left(\frac{\nu}{U_e \delta}\right)^{\frac{1}{4}}$$

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Zero pressure gradient (flat plate) boundary-layer

- Assuming turbulent flow from $x=0$ ($\delta=0$)

$$\frac{\delta}{x} = 0,37R_{e_x}^{-1/5} \qquad \frac{\delta^*}{x} = 0,046R_{e_x}^{-1/5}$$

$$\frac{\theta}{x} = 0,036R_{e_x}^{-1/5} \qquad H = 1,29$$

$$C_f = 0,0576R_{e_x}^{-1/5} \qquad C_D = 0,072R_{e_x}^{-1/5}$$

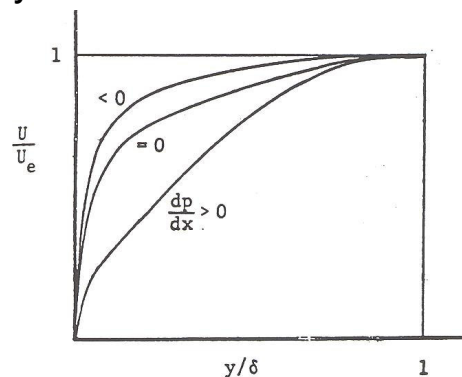
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Effect of the pressure gradient

- Qualitatively, the effect is similar to that discussed previously for laminar flow



- H decreases for favourable pressure gradient and it increases for adverse pressure gradient

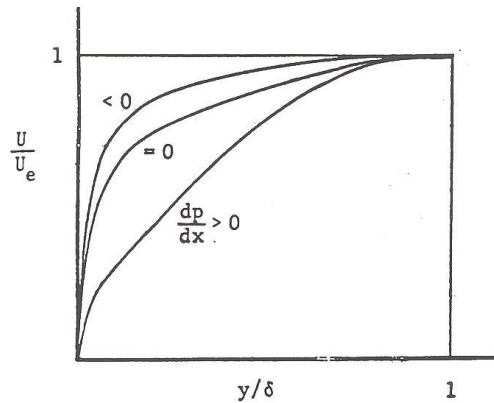
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Effect of the pressure gradient

- Entrainment is strongly dependent on the gradients of the mean velocity profile in the outer region of the boundary-layer (production of turbulence kinetic energy is proportional to the gradients of the mean velocity)

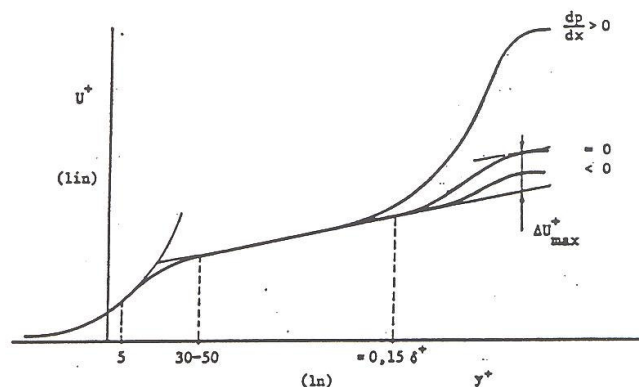


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Effect of the pressure gradient

- Effect on the wall (log) law



- Validity of wall (log) law at flow separation is extremely doubtful

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Effect of the pressure gradient

- Turbulent flow is significantly more resistant to flow separation than laminar flow.
 1. Velocity close to the wall is larger than in laminar flow
 2. Diffusion is significantly higher than in laminar flow (separation depends on the ratio between the pressure force and diffusion)

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Head's method

- von Kármán's integral equation

$$\frac{d\theta}{dx} + \theta \frac{H+2}{U_e} \frac{dU_e}{dx} = \frac{C_f}{2}$$

- Entrainment velocity, V_E

$$V_E = \frac{d}{dx} \int_0^\delta U dy = \frac{d}{dx} [U_e (\delta - \delta^*)]$$

- Shape parameter, H_1

$$H_1 = \frac{\delta - \delta^*}{\theta}$$

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Head's method

- Additional equation proposed

$$\frac{d}{dx}(U_e \theta H_1) = U_e F(H_1) \quad H_1 = G(H)$$

- Experimental fit to determine $F(H_1)$ and $G(H)$

$$F(H_1) = 0,0306(H_1 - 3)^{-0,6169}$$
$$H_1 = G(H) = \begin{cases} 0,8234(H - 1,1)^{-1,287} + 3,3 & \Leftarrow H \leq 1,6 \\ 1,5501(H - 0,6778)^{-3,064} + 3,3 & \Leftarrow H > 1,6 \end{cases}$$

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Head's method

- Ludwig-Tillman correlation to determine C_f

$$C_f = 0,246 \times 10^{-0,678H} \times R_{e\theta}^{-0,268}$$

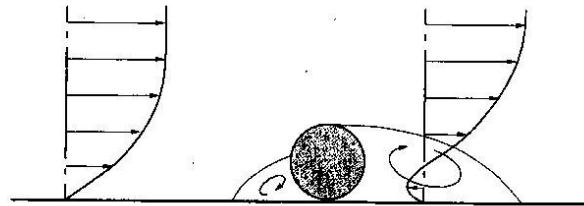
- Flow separation predicted for $H \approx 2.4 - 2.8$
- Numerical solution with a Runge-Kutta scheme

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Turbulent Flow

Boundary-layer control

- Forced transition: roughness or trip wire
The objective is to delay or avoid flow separation

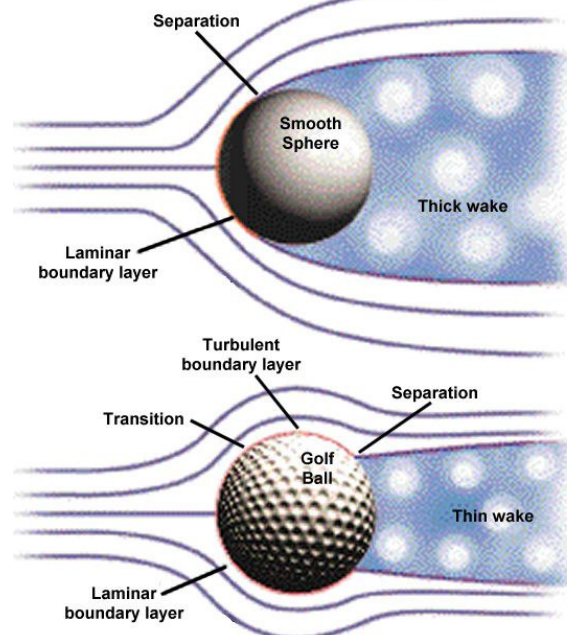


$$R_{e_{arame}} = \frac{U_e d_{arame}}{\nu} \geq 826 \quad \text{Gibbings's criterion}$$

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Turbulent Flow

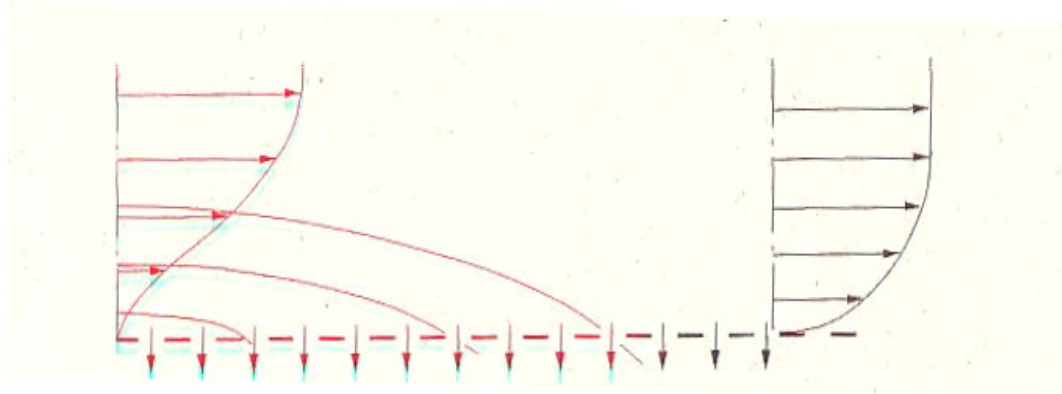
Boundary-layer control



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Turbulent Flow Boundary-layer control

- Suction at the wall. Delays (or avoids) flow separation and it also delays transition from laminar to turbulent flow

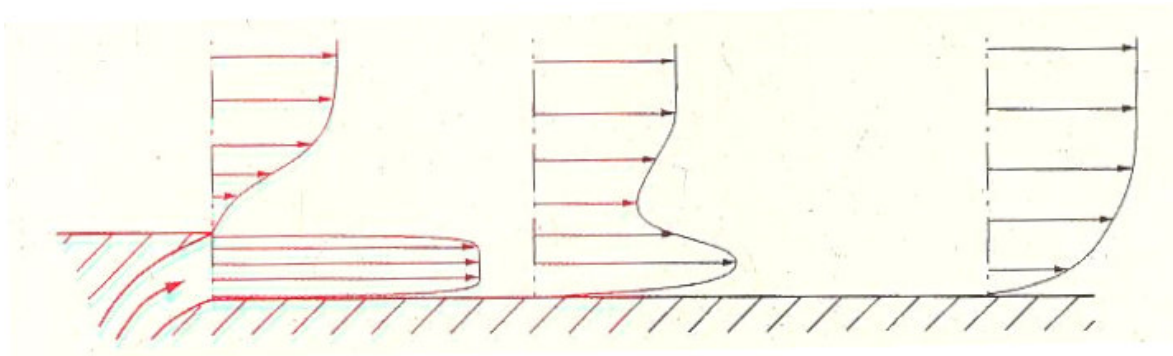


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Turbulent Flow Boundary-layer control

- Blowing. Delays or avoids flow separation, but it favours transition from laminar to turbulent flow



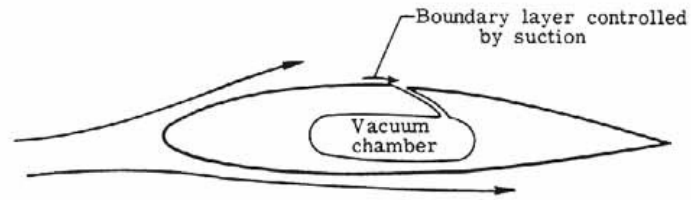
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Turbulent Flow

Boundary-layer control



(a) Suction of boundary layer.



(b) Reenergizing the boundary layer.