

Aerodynamics
Turbulent Flow
Reynolds-averaged (RANS) equations

- Time averaging applied to the dependent variables and to “conservation” principles

$$\overline{\tilde{\phi}_i} = \lim_{T \rightarrow \infty} \frac{\int_{t_0}^{t_0+T} \tilde{\phi}_i dt}{T} = \Phi_i$$

$\tilde{\phi}_i$ stands for any of the dependent variables
(incompressible flow u, v, w, p)

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- Decomposition of the instantaneous variables

$$\tilde{\phi} = \Phi_i + \phi_i$$

$\tilde{\phi}$ → Instantaneous variable

Φ_i → Mean value

ϕ_i → Fluctuation around the mean value

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- Consequences of time averaging

$$\frac{\partial \Phi}{\partial t} = 0 \rightarrow \text{Time derivative of mean value is zero}$$

$$\left. \begin{array}{l} \frac{\partial \phi}{\partial t} = 0 \rightarrow \\ \frac{\partial \phi}{\partial x_i} = 0 \rightarrow \end{array} \right\} \text{Mean value of the time derivative of the} \\ \text{fluctuations is zero}$$

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- Linear terms

$$\frac{\partial \tilde{\phi}}{\partial t} = \frac{\partial \Phi}{\partial t} + \frac{\partial \phi}{\partial t} \Rightarrow \overline{\frac{\partial \tilde{\phi}}{\partial t}} = 0$$

$$\frac{\partial \tilde{\phi}}{\partial x_i} = \frac{\partial \Phi}{\partial x_i} + \frac{\partial \phi}{\partial x_i} \Rightarrow \overline{\frac{\partial \tilde{\phi}}{\partial x_i}} = \frac{\partial \Phi}{\partial x_i}$$

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- Non-linear terms

$$\tilde{u} \frac{\partial \tilde{\phi}_i}{\partial x} + \tilde{v} \frac{\partial \tilde{\phi}_i}{\partial y} + \tilde{w} \frac{\partial \tilde{\phi}_i}{\partial z} = \frac{\partial \tilde{u} \tilde{\phi}_i}{\partial x} + \frac{\partial \tilde{v} \tilde{\phi}_i}{\partial y} + \frac{\partial \tilde{w} \tilde{\phi}_i}{\partial z}$$

$$\overline{\frac{\partial \tilde{u}_j \tilde{\phi}_i}{\partial x_j}} = U_i \frac{\partial \Phi_j}{\partial x_j} + \overline{\frac{\partial u \phi}{\partial x_j}}$$

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- Continuity equation

$$\frac{\partial U}{\partial x} + \frac{\partial V}{\partial y} + \frac{\partial W}{\partial z} = 0$$

- Velocity fluctuations also satisfy

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

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• Momentum equations

$$U \frac{\partial U}{\partial x} + V \frac{\partial U}{\partial y} + W \frac{\partial U}{\partial z} = -\frac{1}{\rho} \frac{\partial P}{\partial x} + \frac{\partial}{\partial x} \left(\nu \frac{\partial U}{\partial x} - \overline{uu} \right) + \frac{\partial}{\partial y} \left(\nu \frac{\partial U}{\partial y} - \overline{uv} \right) + \frac{\partial}{\partial z} \left(\nu \frac{\partial U}{\partial z} - \overline{uw} \right)$$

$$U \frac{\partial V}{\partial x} + V \frac{\partial V}{\partial y} + W \frac{\partial V}{\partial z} = -\frac{1}{\rho} \frac{\partial P}{\partial y} + \frac{\partial}{\partial x} \left(\nu \frac{\partial V}{\partial x} - \overline{vu} \right) + \frac{\partial}{\partial y} \left(\nu \frac{\partial V}{\partial y} - \overline{vv} \right) + \frac{\partial}{\partial z} \left(\nu \frac{\partial V}{\partial z} - \overline{vw} \right)$$

$$U \frac{\partial W}{\partial x} + V \frac{\partial W}{\partial y} + W \frac{\partial W}{\partial z} = -\frac{1}{\rho} \frac{\partial P}{\partial z} + \frac{\partial}{\partial x} \left(\nu \frac{\partial W}{\partial x} - \overline{wu} \right) + \frac{\partial}{\partial y} \left(\nu \frac{\partial W}{\partial y} - \overline{wv} \right) + \frac{\partial}{\partial z} \left(\nu \frac{\partial W}{\partial z} - \overline{ww} \right)$$

- $-\rho \overline{u_i u_j}$ Reynolds stresses
- The number of equations is smaller than the number of unknowns

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 Reynolds-averaged (RANS) equations

 • Transport equation of $-\rho \overline{u_i u_j}$

$$\begin{aligned} \frac{D \overline{u_i u_j}}{Dt} = \frac{\partial \overline{u_i u_j}}{\partial t} + U_k \frac{\partial \overline{u_i u_j}}{\partial x_k} = & - \left(\overline{u_i u_j} \frac{\partial U_i}{\partial x_k} + \overline{u_i u_k} \frac{\partial U_j}{\partial x_k} \right) + \frac{p}{\rho} \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \\ & - \frac{\partial}{\partial x_k} \left(\overline{u_i u_j u_k} \right) - \frac{1}{\rho} \left(\frac{\partial \overline{p u_j}}{\partial x_i} + \frac{\partial \overline{p u_i}}{\partial x_j} \right) \\ & + \nu \frac{\partial^2 \overline{u_i u_j}}{\partial x_i^2} - 2\nu \frac{\partial u_i}{\partial x_k} \frac{\partial u_j}{\partial x_k} \end{aligned}$$

- System remains with less equations than unknowns

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Turbulent Flow

Reynolds-averaged (RANS) equations

- Reynolds stress models
 - 6 additional transport equations
 - Most of the terms of the Reynolds stresses transport equations must be modeled, including pressure fluctuations
 - There are alternative Explicit Algebraic Stress Models (EASMs) available
 - Turbulence anisotropy is taken into account

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Turbulent Flow

Reynolds-averaged (RANS) equations

- Eddy-viscosity models
 - Boussinesq hypothesis: the Reynolds stresses are proportional to mean velocity derivatives
 - The proportionality constant is the eddy-viscosity
 - It is difficult to include the anisotropy of turbulence. Most models are isotropic, i.e. eddy-viscosity is a scalar quantity

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Turbulent Flow Reynolds-averaged (RANS) equations

- Momentum equations including an effective viscosity

$$U \frac{\partial U}{\partial x} + V \frac{\partial U}{\partial y} + W \frac{\partial U}{\partial z} = -\frac{1}{\rho} \frac{\partial P}{\partial x} + 2 \frac{\partial}{\partial x} \left(\nu_{ef} \frac{\partial U}{\partial x} \right) + \frac{\partial}{\partial y} \left(\nu_{ef} \left(\frac{\partial U}{\partial y} + \frac{\partial V}{\partial x} \right) \right) + \frac{\partial}{\partial z} \left(\nu_{ef} \left(\frac{\partial U}{\partial z} + \frac{\partial W}{\partial x} \right) \right)$$

$$U \frac{\partial V}{\partial x} + V \frac{\partial V}{\partial y} + W \frac{\partial V}{\partial z} = -\frac{1}{\rho} \frac{\partial P}{\partial y} + \frac{\partial}{\partial x} \left(\nu_{ef} \left(\frac{\partial U}{\partial y} + \frac{\partial V}{\partial x} \right) \right) + 2 \frac{\partial}{\partial y} \left(\nu_{ef} \frac{\partial V}{\partial y} \right) + \frac{\partial}{\partial z} \left(\nu_{ef} \left(\frac{\partial V}{\partial z} + \frac{\partial W}{\partial y} \right) \right)$$

$$U \frac{\partial W}{\partial x} + V \frac{\partial W}{\partial y} + W \frac{\partial W}{\partial z} = -\frac{1}{\rho} \frac{\partial P}{\partial z} + \frac{\partial}{\partial x} \left(\nu_{ef} \left(\frac{\partial U}{\partial z} + \frac{\partial W}{\partial x} \right) \right) + \frac{\partial}{\partial y} \left(\nu_{ef} \left(\frac{\partial V}{\partial z} + \frac{\partial W}{\partial y} \right) \right) + 2 \frac{\partial}{\partial z} \left(\nu_{ef} \frac{\partial W}{\partial z} \right)$$

$$\nu_{ef} = \nu + \nu_t$$

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Turbulent Flow Reynolds-averaged (RANS) equations

- Momentum equations including an effective viscosity

– ν_t is the eddy-viscosity

- Eddy-viscosity is obtained from velocity and length scales of turbulence

- Several models proposed in the last 50 years

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Turbulent Flow

Reynolds-averaged (RANS) equations

- Eddy-viscosity turbulence models
 - Algebraic models
 - Turbulence length scale
 $l = \kappa y \rightarrow$ Mixing length
 - Turbulence velocity scale
 $l|\vec{\omega}| \rightarrow \vec{\omega}$ is the vorticity vector
 $\nu_t = l^2|\vec{\omega}|$

Turbulent Flow

Reynolds-averaged (RANS) equations

- Eddy-viscosity turbulence models
 - Algebraic models
 - Damping function is applied to the turbulence length scale in the near-wall region. Length scale must be changed for the outer region of the boundary-layer, wakes and jets
 - Simplest model available, but with severe limitations. Numerical implementation in complex flows may be troublesome

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 Turbulent Flow
 Reynolds-averaged (RANS) equations

- Eddy-viscosity turbulence models
 - 1-equation models (“old style”)
 - Turbulence length scale is identical to that used in the algebraic models
 - Turbulence velocity scale is the square root of the turbulence kinetic energy, which has its own transport equation

$$k = \frac{1}{2} \overline{u^2 + v^2 + w^2}$$

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 Turbulent Flow
 Reynolds-averaged (RANS) equations

- Turbulence kinetic energy, k
 - Transport equation (k balance)

$$\begin{aligned} \frac{Dk}{Dt} = \frac{\partial k}{\partial t} + U_j \frac{\partial k}{\partial x_j} = & - \left(\overline{u_i u_j} \frac{\partial U_i}{\partial x_j} \right) - \frac{\partial}{\partial x_j} \left(\frac{1}{\rho} \overline{p u_j} + \frac{1}{2} \overline{u_i u_i u_j} \right) \\ & + \nu \frac{\partial^2 k}{\partial x_j^2} - \nu \left(\overline{\frac{\partial u_i}{\partial x_j}} \right)^2 \end{aligned}$$

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Turbulent Flow
Reynolds-averaged (RANS) equations

- Turbulence kinetic energy, k

$$U_j \frac{\partial k}{\partial x_j} \rightarrow \text{Convection}$$

$$-\left(\overline{u_i u_j} \frac{\partial U_i}{\partial x_j}\right) \rightarrow \text{Production}$$

$$-\frac{\partial}{\partial x_j} \left(\frac{1}{\rho} \overline{p u_j} + \frac{1}{2} \overline{u_i u_i u_j} \right) \rightarrow \text{Turbulent diffusion}$$

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Turbulent Flow
Reynolds-averaged (RANS) equations

- Turbulence kinetic energy, k

$$\nu \frac{\partial^2 k}{\partial x_j^2} \rightarrow \text{Viscous diffusion}$$

$$-\nu \left(\overline{\frac{\partial u_i}{\partial x_j}} \right)^2 \rightarrow \text{Dissipation rate, } \varepsilon$$

- Most of the terms include unknown quantities and so they must be modeled

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Turbulent Flow
Reynolds-averaged (RANS) equations

- Eddy-viscosity turbulence models
 - 1-equations models

Spalart & Allmaras $\nu_t = f_{v1} \tilde{\nu}$

$$U \frac{\partial \tilde{\nu}}{\partial x} + V \frac{\partial \tilde{\nu}}{\partial y} = c_{b1} \tilde{\nu} \tilde{S} + \frac{1}{\sigma_s} [\nabla \cdot (\nu + \tilde{\nu}) \nabla \tilde{\nu} + c_{b2} (\nabla \tilde{\nu} \cdot \nabla \tilde{\nu})] - c_{w1} f_w \left(\frac{\tilde{\nu}}{d} \right)^2$$

 $c_{b1}, c_{b2}, c_{w1} \rightarrow$ Constants $f_{v1}, f_w \rightarrow$ Functions

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Turbulent Flow
Reynolds-averaged (RANS) equations

- Eddy-viscosity turbulence models
 - 1-equation model of Spalart & Allmaras
 - Valid down to the wall
 - Eddy-viscosity is proportional to the dependent variable of the model
 - It requires the distance to the wall, d , and in its original version the location of transition

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Turbulent Flow
Reynolds-averaged (RANS) equations

• Eddy-viscosity turbulence models

- 2-equation models: turbulence velocity scale is \sqrt{k}

- k - ε model $\nu_t = C_\mu \frac{k^2}{\varepsilon}$

$$U \frac{\partial k}{\partial x} + V \frac{\partial k}{\partial y} = \nu_t S^2 + \nabla \cdot \left(\left(\nu + \frac{\nu_t}{\sigma_k} \right) \nabla k \right) - \varepsilon$$

$$U \frac{\partial \varepsilon}{\partial x} + V \frac{\partial \varepsilon}{\partial y} = C_1 \frac{\varepsilon}{k} \nu_t S^2 + \nabla \cdot \left(\left(\nu + \frac{\nu_t}{\sigma_\varepsilon} \right) \nabla \varepsilon \right) - C_2 \frac{\varepsilon^2}{k}$$

$C_\mu, C_1, C_2, \sigma_k, \sigma_\varepsilon \rightarrow$ Constants

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Turbulent Flow
Reynolds-averaged (RANS) equations

• Eddy-viscosity turbulence models

- k - ε model

- Widely used, specially in flows without walls and in heat transfer problems

- Poor results for flows with adverse pressure gradients

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 Turbulent Flow
 Reynolds-averaged (RANS) equations

- Eddy-viscosity turbulence models
 - k - ε model
 - Can not be applied in the near-wall region
 - Two-layer models combine the k - ε model in the outer region with a 1-equation model in the near-wall region
 - There are (too many) Low-Reynolds number versions of the model for its extension to the near-wall region

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 Turbulent Flow
 Reynolds-averaged (RANS) equations

- Eddy-viscosity turbulence models

- k - ω model $\nu_t = \frac{k}{\omega}$

$$U \frac{\partial k}{\partial x} + V \frac{\partial k}{\partial y} = \nu_t S^2 + \nabla \cdot \left(\left(\nu + \frac{\nu_t}{\sigma_k} \right) \nabla k \right) - \beta^* \omega k$$

$$U \frac{\partial \omega}{\partial x} + V \frac{\partial \omega}{\partial y} = \alpha S^2 + \nabla \cdot \left(\left(\nu + \frac{\nu_t}{\sigma_\omega} \right) \nabla \omega \right) - \frac{F_\omega}{\omega} (\nabla k \cdot \nabla \omega) - \beta \omega^2$$

$$\beta^*, \beta, \alpha, \sigma_k, \sigma_\omega \rightarrow \text{Constants} \quad F_\omega \rightarrow \text{Function}$$

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Turbulent Flow
Reynolds-averaged (RANS) equations

- Eddy-viscosity turbulence models
 - $k-\omega$ model
 - May be applied down to the wall
 - ω goes to infinity at the wall (smooth walls)
 - Several formulations available. One of the most popular is the SST (Shear-Stress Transport) version that includes a limiter for the eddy-viscosity

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Turbulent Flow
Reynolds-averaged (RANS) equations

- Eddy-viscosity turbulence models
 - $k-\omega$ model
 - Widely used for the calculation of adverse pressure gradient flows
 - Numerical implementation is not trivial (w wall boundary condition) and some versions (as for example SST) require the distance to the wall

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